

Solutions to Homework Assignment #1

1. **Explain how a high-gain feedback loop can be used to produce an implicit inverse of the plant model. (20 pts)**

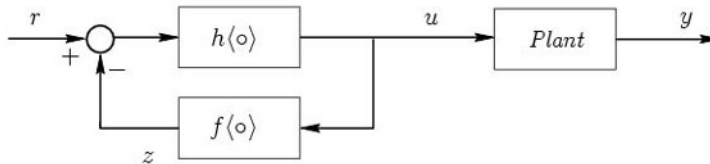


Figure 2.7:
*Realisation of
conceptual controller*

From Fig. 2.7 of Goodwin et al., $u = h\langle r - z \rangle = h\langle r - f\langle u \rangle \rangle$. Passing each side of this equation through the function $h^{-1}\langle \circ \rangle$ gives $h^{-1}\langle u \rangle = r - f\langle u \rangle$ or $f\langle u \rangle = r - h^{-1}\langle u \rangle$. Passing each side of this last equation through the function $f^{-1}\langle \circ \rangle$ then gives $u = f^{-1}\langle r - h^{-1}\langle u \rangle \rangle$. If $h^{-1}\langle u \rangle \ll r$, then $u \approx f^{-1}\langle r \rangle$. That is, the feedback loop produces an approximate inverse of $f\langle \circ \rangle$ under the condition that $h^{-1}\langle \circ \rangle$ is small, i.e., the gain of $h\langle \circ \rangle$ is high.

2. **List under what conditions might an open-loop controller be acceptable? Describe the advantages of using an open-loop controller as compared to a closed-loop controller such a case? (20 pts)**

An open-loop controller may be sufficient if:

- a very accurate model of the plant is known,
- the model and its inverse are stable, and
- disturbances and initial conditions are negligible.

The advantages of an open-loop controller are:

- no sensors required,
- the controller may be reducible to a very simple system (e.g., an IIR filter), and
- no transmission of sensor information required, and consequently a possible source of signal delay is removed.

3. **Explain why a closed-loop controller is preferable to an open-loop controller for most control problems? (20 pts)**

Closed-loop controllers are more forgiving in the presence of modelling errors, system instabilities, unknown initial conditions and disturbances to any signal in the system, because the *actual* output of the plant is being taken into account when producing the control signal.

4. A nonlinear system has an input-output model given by:

$$\frac{dy(t)}{dt} + (1 + 0.2y(t))y(t) = u(t) + 0.2u(t)^3$$

- a. Compute the operating points, i.e., values of y for a particular value of u , for $u_Q = 2$. (assume they are equilibrium points, i.e., $\frac{dy(t)}{dt} = 0$)
- b. Obtain a linearized model for each of the operating points above. (40 pts)

- a. If $\frac{dy(t)}{dt} = 0$ and $u_Q = 2$, then $0.2y_Q^2 + y_Q = u_Q + 0.2u_Q^3 \Rightarrow 0.2y_Q^2 + y_Q - 3.6 = 0$ and consequently $y_Q = -7.4244$ or 2.4244 .
- b. The system can be linearized by using the first-order Taylor series to approximate the model, such that:

$$\frac{d\Delta y(t)}{dt} \approx \left. \frac{\partial f}{\partial y} \right|_{\substack{y=y_Q \\ u=u_Q}} \Delta y(t) + \left. \frac{\partial f}{\partial u} \right|_{\substack{y=y_Q \\ u=u_Q}} \Delta u(t),$$

where $\Delta y(t) = y(t) - y_Q$ and $\Delta u(t) = u(t) - u_Q$.

Solving this equation for the nonlinear model gives the linear equation:

$$\frac{d\Delta y(t)}{dt} + (1 + 0.4y_Q)\Delta y(t) = (1 + 0.6u_Q^2)\Delta u(t).$$

For the two equilibrium points $(u_Q, y_Q) = (2, -7.4244)$ and $(2, 2.4244)$ obtained in part a. above, the system can be modelled, respectively, as:

$$\frac{d\Delta y(t)}{dt} - 1.9698\Delta y(t) = 3.4\Delta u(t), \text{ and}$$

$$\frac{d\Delta y(t)}{dt} + 1.9698\Delta y(t) = 3.4\Delta u(t).$$